Table I. Vapor Pressures Derived from $U^{(2)}$ and from Published Data [10] for R41.

T (K)	P_σ[a] (Pa)	$P_{\sigma,published}$ (Pa)	$P_\sigma - P_{\sigma,published}$ (Pa)
129.82	321.9	346.4	-24.5
130	330.3	355.1	-24.8
135	651.4	685.7	-34.3
140	1212.4	1255.4	-43.0
145	2143.9	2192.6	-48.7
150	3623.6	3671.8	-48.2
155	5883.6	5922.0	-38.4
160	9217.7	9234.2	-16.5
165	13987.1	13968.1	19.0
170	20625.4	20557.5	67.9
175	29642.0	29513.9	128.1
180	41623.9	41428.9	195.0
185	57237.5	56975.0	262.5
190	77227.7	76905.5	322.2
195	102417.7	102052.0	365.7
200	133707.6	133322.6	385.0
205	172071.7	171698.0	373.7
210	218556.8	218228.1	328.7
215	274279.1	274028.0	251.1
220	340421.9	340274.3	147.6
225	418232.4	418201.3	31.1
230	509019.5	509098.7	-79.2
235	614151.2	614308.9	-157.7
240	735053.2	735226.4	-173.2
245	873206.9	873297.7	-90.8
250	1030149.0	1030023.0	126.0

[a] The number of figures presented is for comparison only.

Table II. Vapor Pressures Derived from $U^{(2)}$ and from Published Data [12] for R152a.

T (K)	P_σ (Pa)	$P_{\sigma,published}$ (Pa)	P_σ - $P_{\sigma,published}$ (Pa)
154.56	64.0	64.1	-0.1
155	67.9	68.0	-0.1
160	129.7	129.9	-0.2
165	236.8	237.0	-0.2
170	414.8	415.0	-0.2
175	700.0	700.1	-0.1
180	1142.0	1141.9	0.1
185	1806.3	1805.8	0.5
190	2777.5	2776.2	1.3
195	4162.0	4159.6	2.4
200	6090.7	6086.6	4.1
205	8721.3	8715.0	6.3
210	12240.5	12231.4	9.1
215	16865.7	16853.1	12.6
220	22846.2	22829.6	16.6
225	30464.1	30442.8	21.3
230	40034.3	40008.2	26.1
235	51905.0	51874.3	30.7
240	66457.2	66422.3	34.9
245	84103.7	84065.6	38.1
250	105288.4	105249.0	39.4

Table III. Vapor Pressures Derived from $U^{(2)}$ and from Published Data [18] for R143a.

T (K)	P_σ (Pa)	$P_{\sigma,published}$ (Pa)	P_σ - $P_{\sigma,published}$ (Pa)
161.34	1076.8	1078.0	-1.2
165	1560.0	1560.4	-0.4
170	2511.7	2510.5	1.2
175	3917.7	3913.8	3.9
180	5937.1	5929.5	7.6
185	8764.4	8752.0	12.4
190	12632.2	12614.2	18.0
195	17813.2	17789.0	24.2
200	24621.3	24591.1	30.2
205	33412.5	33377.1	35.4
210	44585.0	44545.7	39.3
215	58578.3	58536.8	41.5
220	75872.6	75830.2	42.4
225	96987.4	96944.4	43.0
230	122479.8	122434.5	45.3

Table IV. Coefficients Obtained with the Present Technique for Vapor-Pressure Ancillary Equations of R41, R152a, and R143a.[a]

	C_1	C_2	C_3	C_4	C_5
Eq. (4), R41	-6.89372992	0.994098037	-1.00720506	-4.39293522	
Eq. (8), R152a	-7.44858013	2.09934200	-1.58655560	-2.82734307	-0.952562831
Eq. (8), R143a	-7.06302701	0.832358227	-0.234939234	-3.59058034	-0.118184722

[a] Coefficients and their respective equations should be applied only within the temperature ranges presented in Tables I, II, and III.

Table V. Vapor Presssure at the Triple Point Temperature for Selected Hydrofluorocarbons.

Substance	T_{tp} (K)	This Method (Pa)	Experimental (Pa)	Ancillary Equation (Pa)	Tilner-Roth Method[21] (Pa)
R125	172.52	2915.6 [1]	n.a.	2953.1 [22]	2921.0
R32	136.34	46.5 [1]	n.a.	46.9 [22]	48.0
R143a	161.34	1076.8	n.a.	1078.0 [18]	1061.0
R134a	169.85	390.2[1]	n.a.	393.4 [23]	392.4
R152a	154.56	64.0	65.0[f]	64.1[12]	64.1
R41	129.82	321.9	n.a.	346.4 [10]	n.a.